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Combined high-power ultrasound and high-pressure homogenization nanoemulsification: The effect of energy density, oil content and emulsifier

Original

Availability:

This version is available <http://hdl.handle.net/11390/1135446> since 2020-02-27T15:32:52Z

Publisher:

Published

DOI:10.1016/j.foodres.2018.03.017

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Manuscript Number: FOODRES-D-17-03013R1

Title: Combined high-power ultrasound and high-pressure homogenization nanoemulsification: the effect of energy density, oil content and emulsifier type and content

Article Type: Research Paper

Keywords: high-power ultrasound, high-pressure homogenization, combined technologies, energy reduction, nanoemulsion, food emulsifiers.

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Abstract: Combinations of ultrasound (US) and high-pressure homogenization (HPH) at low-medium energy densities were studied as alternative processes to individual US and HPH to produce Tween 80 and whey protein stabilized nanoemulsions, while reducing the energy input. To this aim, preliminary trials were performed to compare emulsification efficacy of single and combined HPH and US treatments delivering low-medium energy densities. Results highlighted the efficacy of US-HPH combined process in reducing the energy required to produce nanoemulsions stabilized with both Tween 80 and whey protein isolate. Subsequently, the effect of emulsifier content (1-3% w/w), oil amount (10-20% w/w) and energy density (47-175 MJ/m³) on emulsion mean particle diameter was evaluated by means of a central composite design. Particles of 140-190 nm were obtained by delivering 175 MJ/m³ energy density at emulsions containing 3% (w/w) Tween 80 and 10% (w/w) oil. In the case of whey protein isolate stabilized emulsions, a reduced emulsifier amount (1%, w/w) and intermediate energy density (120 MJ/m³) allowed a minimum droplet size around 220-250 nm to be achieved. Results showed that, in both cases, at least 50% of the energy density should be delivered by HPH to obtain the minimum particle diameter.

Dear Editor,

I would like to submit to your attention the manuscript entitled “Combined high-power ultrasound and high-pressure homogenization nanoemulsification: the effect of energy density, oil content and emulsifier type and content” (Authors: Sonia Calligaris, Stella Plazzotta, Fabio Valoppi, Monica Anese) for consideration for publication on Food Research International.

Recently, we have demonstrated that combined US-HPH processes can be effective in reducing the energy demand for nanoemulsion preparation by using a combination of synthetic surfactants (Tween 80 and Span 80) with well-known excellent performances under high-energy emulsification (Calligaris et al., 2016 Food Research International 83, 25-30). In particular, US and HPH provided in combination at low and medium energy density values led to nanoemulsions with particle size and stability comparable to those prepared by using individual US or HPH at high energy densities. The aim of this work was to investigate further US-HPH nanoemulsification in obtaining nanoemulsions in the presence of food grade emulsifiers. To this purpose, preliminary trials were carried out to evaluate the effectiveness of US-HPH combined processes to obtain nanoemulsions containing Tween 80 or whey proteins as emulsifiers. Then, a three-variable face centred central composite design was used to study the effect of emulsifier content (1-3% w/w), oil amount (10-20% w/w) and energy density (48-175 MJ/m³) on emulsion mean particle diameter. Finally, the effect of different US and HPH combinations developing the same energy density was studied to identify the optimal energy share between US and HPH allowing minimum droplet diameter to be obtained during a combined process.

Results confirmed the efficacy of US-HPH combined process in reducing the energy required to produce nanoemulsions stabilized with both Tween 80 and whey protein isolate. However, different performances should be expected depending on the emulsifier used. Particles of 140-190 nm were obtained by delivering 175 MJ/m³ energy density at emulsions containing 3% (w/w) Tween 80 and 10% (w/w) oil. In the case of whey protein isolate stabilized emulsions, a reduced emulsifier amount (1%, w/w) and intermediate energy density (120 MJ/m³) allowed a minimum droplet size around 220-250 nm to be achieved. Results showed that, in both cases, at least 50% of the energy density should be delivered by HPH to obtain the minimum particle diameter.

Best regards,
Sonia Calligaris

Dear Editor,

We send to your attention the research article entitled "**Combined high-power ultrasound and high-pressure homogenization nanoemulsification: the effect of energy density, oil content and emulsifier type and content**". We have endeavoured to take into account or to respond to the Associate editor's and Reviewer's comments as indicated below.

We hope that this response is satisfactory and that the manuscript will be suitable for publication in Food Research International.

Best regards

Sonia Calligaris

Associated Editor Comments

Although the paper is really interesting, R&D, especially discussion section should be improved to explain the impact of energy density, oil content and emulsifier type and content.

Answer: The R&D part of the manuscript has been deeply revised including more discussion to explain the effects of different variables on nanoemulsion properties (section 3.2 and 3.3).

Reviewer #3:

The present paper involves a comprehensive research about the use of combined high pressure homogenization and ultrasounds to obtain stable nanoemulsions with a lower energy density process.

Several previous works have carried out related experiments, and have already dealt with the use of high pressure homogenization and ultrasounds for nanoemulsion obtaining, already cited in the text. Consequently, results presented in this work expand previous knowledge with new conditions and a more inclusive selection of variables (emulsifier content and type, oil content...). These data seem to be useful for optimization of a putative industrial process, thus its novelty is justified.

The paper is well written, results are interesting, data appear well presented and properly related, but I miss more discussion of the results. E.g.: sections 3.2 and 3.3 are only "results", not "results and discussion". Accordingly, some changes and considerations should be taken into account previously to its publication in the current form.

Answer: We thank the reviewer for the appreciation of the manuscript. As suggested, the R&D part of the manuscript (section 3.2 and 3.3) has been deeply revised including more discussion to explain the effects of different variables on nanoemulsion properties.

MINOR REVISIONS

In general, please, be careful with text presentation. In many cases, some words are written together or there is no space after a dot. Some examples:

line 195: 150MPafor, at120MPa

line 196: from20 to...

line 206: bythe

Answer: We carefully check the text to delete errors.

RESULTS AND DISCUSSION:

Please, provide some discussion for the results in sections 3.2 and 3.3.

Answer: see above

REFERENCES:

Line 344: The reference (Floury et al., 2002) is not cited in the text. Delete or cite.

Line 350: The reference (Hulsmans et al., 2010) is not cited in the text. Delete or cite.

Answer: references were deleted.

Highlights

Combined US-HPH process allowed obtaining nanoemulsions using food grade emulsifiers

US-HPH process allowed nanoemulsification energy density to be reduced

Oil and emulsifier content and energy density affected US-HPH emulsification efficacy

US and HPH energy levels affected US-HPH nanoemulsification performance

1 **Combined high-power ultrasound and high-pressure homogenization nanoemulsification: the**
2 **effect of energy density, oil content and emulsifier type and content**

3

4 **Sonia Calligaris*, Stella Plazzotta, Fabio Valoppi, Monica Anese**

5

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11 **Abstract**

12 Combinations of ultrasound (US) and high-pressure homogenization (HPH) at low-medium energy
13 densities were studied as alternative processes to individual US and HPH to produce Tween 80 and
14 whey protein stabilized nanoemulsions, while reducing the energy input. To this aim, preliminary
15 trials were performed to compare emulsification efficacy of single and combined HPH and US
16 treatments delivering low-medium energy densities. Results highlighted the efficacy of US-HPH
17 combined process in reducing the energy required to produce nanoemulsions stabilized with both
18 Tween 80 and whey protein isolate. Subsequently, the effect of emulsifier content (1-3% w/w), oil
19 amount (10-20% w/w) and energy density (47-175 MJ/m³) on emulsion mean particle diameter was
20 evaluated by means of a central composite design. Particles of 140-190 nm were obtained by
21 delivering 175 MJ/m³ energy density at emulsions containing 3% (w/w) Tween 80 and 10% (w/w)
22 oil. In the case of whey protein isolate stabilized emulsions, a reduced emulsifier amount (1% w/w)
23 and intermediate energy density (120 MJ/m³) allowed a minimum droplet size around 220-250 nm
24 to be achieved. Results showed that, in both cases, at least 50% of the energy density should be
25 delivered by HPH to obtain the minimum particle diameter.

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Keywords: high-power ultrasound, high-pressure homogenization, combined technologies, energy
reduction, nanoemulsion, food emulsifiers.

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33 **1. Introduction**

34 The interest in food grade nanoemulsions has rapidly increased in the last decades, due to their
35 unique physico-chemical properties and possible application as delivery systems of bioactive
36 molecules (Karthik, Ezhilarasi, & Anandharamakrishnan, 2017; Sanguansri & Augustin, 2006).
37 Nanoemulsions are heterogeneous systems consisting of two immiscible liquids, with one phase
38 being dispersed as nanometric droplets with diameter lower than 200 nm (Salvia-Trujillo, Soliva-
39 Fortuny, Rojas-Grau, McClements, & Martin-Belloso, 2017). Formation and stabilization of
40 nanoemulsions depend on the physical-chemical properties of constituents, including oil and
41 aqueous phases and emulsifiers, as well as on the energy density, i.e. the energy input per unit
42 volume transferred to the sample. Energy density, in turn, depends on treatment intensity and
43 duration (Mohd-Setapar, Nian-Yian, Nuraisha, Kamarudin, & Idham, 2013; Schubert & Engel,
44 2004; Schubert, Ax, & Behrend, 2003; Stang, Schuchmann, & Schubert, 2001; Wooster, Golding,
45 & Sanguansri, 2008). Smaller droplets are usually obtained by increasing the emulsifier content and
46 the supplied energy density. Also, at comparable energy densities, the modality of energy delivering
47 can affect the nanoemulsion particle size and stability (Calligaris et al., 2016; Jafari, Assadpoor, He,
48 & Bhandari, 2008). Different mechanical devices capable of generating intense disruptive forces
49 can be used to obtain nanoemulsions. High-power ultrasound (US) and high-pressure
50 homogenization (HPH) are high-energy nanoemulsification processes, which are able to reduce the
51 emulsion particle diameter at nano-level (Abbas, Hayat, Karangwa, Bashari, & Zhang, 2013;
52 Canselier, Delmas, Wilhelm, & Abismaïl, 2002; Dumay et al., 2013; McClements, 2005; Silva,
53 Cerqueira, & Vicente, 2012). High-power ultrasonic devices form emulsions with nano-sized
54 droplets through the propagation of low frequency sound waves (20-24 kHz), which cause the
55 formation and violent collapse of cavitation bubbles (Abbas et al., 2013; Leong, Wooster, Kentish,
56 & Ashokkumar, 2009). High-pressure homogenizers break large droplets into smaller ones by a
57 combination of intensive disruptive forces, such as shear stress, cavitation and turbulent flow
58 conditions, suffered by the product during the passage in the homogenization valve (Stang et al.,
59 2001). Both technologies require extremely intense treatments (long times in US and high pressures
60 and/or multiple passes in HPH) to produce emulsions with nano-size droplets (Kentish et al., 2008;
61 McClements & Rao, 2011; Qian & McClements, 2011). This implies the use of specifically
62 designed equipment and relatively high running and maintenance costs, due to elevated energy
63 consumption and frequent replacement of wearing parts. Therefore, the industrial application of US
64 and HPH as high-energy emulsification processes is limited because of their low sustainability.

65 Based on these considerations, the possibility to reduce the energy requirements for
52 nanoemulsification might stir up new interest in large-scale production of nanoemulsions. Recently,
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67 it has been demonstrated that combined US-HPH processes can be effective in reducing the energy
68 demand for nanoemulsion preparation by using a combination of food-grade synthetic surfactants
69 (Tween 80 and Span 80) with well-known excellent performances under high-energy emulsification
70 (Calligaris et al., 2016). In particular, US and HPH provided in combination at low and medium
71 energy density values led to nanoemulsions with particle size and stability comparable to those
72 prepared by using individual US or HPH at high energy densities.

73 The aim of this work was to investigate further US-HPH nanoemulsification in obtaining
74 nanoemulsions in the presence of food grade emulsifiers. To this purpose, preliminary trials were
75 carried out to evaluate the effectiveness of US-HPH combined processes to obtain nanoemulsions
76 containing Tween 80 or whey proteins as emulsifiers. Then, a three-variable face centred central
77 composite design was used to study the effect of emulsifier content (1-3% w/w), oil amount (10-
78 20% w/w) and energy density (48-175 MJ/m³) on emulsion mean particle diameter. Finally, the
79 effect of different US and HPH combinations developing the same energy density was studied to
80 identify the optimal energy share between US and HPH allowing minimum droplet diameter to be
81 obtained during a combined process.

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83 **2. Materials and methods**

84 *2.1. Coarse emulsion preparation*

85 The aqueous phase was prepared by mixing an amount allowing to obtain in the final emulsion 1 to
86 3% (w/w) of Tween 80 (Tween 80®, Sigma Aldrich, Milano, Italy) or whey protein isolate (94.7%
87 protein content; 74.6% β-lactoglobulin, 23.8% α-lactoglobulin, 1.6% bovine serum albumin;
88 Davisco Food International Inc., Le Seur, Germany) with deionized water. The aqueous phase was
89 stirred at 20 °C for 2 h, until the surfactant was completely dissolved. The coarse emulsion was
90 prepared by mixing the aqueous phase with sunflower oil (10-20% w/w) with a high-speed blender
91 (Polytron, PT 3000, Cinematica, Littau, Swiss) at 8000 rpm for 1 min. The coarse emulsion was
92 immediately subjected to the nanoemulsification processes.

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94 *2.2. Nanoemulsification processes*

95 *2.2.1. High-power ultrasound (US)*

96 An ultrasonic processor (Hieschler Ultrasonics GmbH, mod. UP400S, Teltow, Germany) with a
97 titanium horn tip diameter of 22 mm was used. The instrument operated at constant ultrasound
98 amplitude and frequency of 100 μm and 24 kHz, respectively. Aliquots of 150 mL of coarse
509 emulsion were introduced into 250 mL capacity (110 mm height, 60 mm internal diameter) glass
53 vessel. The tip of the sonicator horn was placed in the centre of the solution, with an immersion
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101 depth in the fluid of 50 mm. The ultrasound treatments were performed up to 240 s and the
102 temperature was controlled using a cryostatic cooling system set at 4 °C to dissipate the heat
103 generated during the treatment.

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105 2.2.2. *High-pressure homogenization (HPH)*

106 A continuous lab-scale high-pressure homogenizer (Panda Plus 2000, GEA Niro Soavi, Parma,
107 Italy) supplied with two PS type homogenization valves with a flow rate of 10 L/h was used to treat
108 150 mL of coarse emulsion. The first valve was the actual homogenization stage and was set at
109 increasing pressure up to 150 MPa. The second valve was set at the constant value of 5 MPa.
110 Additional samples were prepared by subjecting the coarse emulsion to HPH for up to 3 successive
111 passes at 120 MPa. At the exit of the homogenizer, the emulsions were forced into a heat exchanger
112 (GEA Niro Soavi, Parma, Italy) and cooled to room temperature.

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114 2.2.3. *Combined US-HPH*

115 The coarse emulsion (150 mL) was subjected to US followed by HPH. The time between the two
116 treatments did not exceed 30s. US treatments were applied for 20 or 60 s, while homogenization
117 pressure was set at 20, 50, 80 and 100 MPa. Further US-HPH treatments consisting of 20 s + 20
118 MPa, 22 s + 80 MPa and 60 s + 100 MPa were carried out to provide energy densities of 47, 111
119 and 175 MJ/m³ according to a central composite design. Finally, to deliver to the sample energy
120 densities of 145 and 120 MJ/m³, the percentage ratio between the energy delivered by US and HPH
121 was progressively changed.

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123 2.3. *Temperature measurement*

124 The sample temperature was measured just before and immediately after (i.e. before the cooling
125 step) HPH process and during US by a copper-constantan thermocouple probe (Ellab, Hillerød,
126 Denmark) connected to a portable data logger (mod. 502A1, Tersid, Milan, Italy).

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128 2.4. *Energy density computation*

129 The energy density, i.e. the energy input per unit volume (E_v , MJ/m³), was computed as described
130 by Bot et al. (2017). In particular, the E_v transferred from the probe to the sample during ultrasound
131 treatments was calculated by using equation (1) (Raso, Mañas, Pagán, & Sala, 1999):

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$$E_v = \frac{mc_p(\partial T / \partial t)}{V} \times t \quad (1)$$

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133 where m is the sample mass (kg), c_p is the sample heat capacity (4186 J/(kg K)), V is the sample
134 volume (cm^3), and t (s) is the duration of the ultrasonication time.

135 The energy density transferred from the valve to the sample during the HPH treatment was
136 determined as described by Stang et al. (2001), according to equation (2):

$$137 \quad E_v = \Delta P \quad (2)$$

138 where ΔP is the pressure difference operating at the nozzles.

139 The energy density of multiple passes HPH and combined treatments was calculated as the sum of
140 the energy density values of the corresponding single pass HPH or US plus HPH treatments.

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142 2.5. Droplet size

143 The mean diameter of emulsion droplets was measured by using the dynamic light scattering
144 instrument Zetasizer Nano ZS (Malvern, Milan, Italy). Samples were diluted 1:10 (v/v) with
145 deionised water prior to the analysis to avoid multiple scattering effects. The angle of observation
146 was 173° . Solution refractive index and viscosity were set at 1.333 and 1.0 cP, respectively,
147 corresponding to the values of pure water at 20°C .

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149 2.6. Polynomial equations and statistical analysis

150 Modelling was aimed at describing the variation of mean particle diameter as a function of the
151 variables of the central composite design. In particular, a 3-factors face centred central composite
152 design (CCF) was used. The three considered factors were oil content, emulsifier concentration and
153 energy density. The ranges of variables were chosen on the basis of information from the
154 preliminary trials, showing that the application of values outside the considered intervals led to non-
155 emulsified samples. For each factor, extreme, lower and upper values were identified and combined
156 to form the factorial part of the design (8 factorial points). In particular, oil content, emulsifier
157 concentration and energy density were set at 10, 15 and 20% (w/w), 1, 2 and 3% (w/w) and 48, 111
158 and 175 MJ/m^3 , respectively. The energy density values were obtained by US-HPH combined
159 treatments of 20 s+20 MPa, 22 s+80 MPa and 60 s+100 MPa. To complete the CCF, 6 axial points
160 (combinations of the extreme value of one factor and the intermediate level for the others) and 1
161 central point (combination of the intermediate values of the three factors) were defined. All the
162 factorial and axial points were replicated once, while the central point was replicated 6 times. The
163 full set of sampling points is reported in Table 1. A software package (Statistica for Windows v. 10,
164 StatSoft, Inc.) was used to fit the second order response surface to the observed data according to
165 the following equation:

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166 $y = B_0 + \sum_{i=1}^k B_i x_i + \sum_{i=1}^k B_{ii} x_i^2 + \sum_{j>i \geq 1}^k B_{ij} x_i x_j$ (3)

167 where B_0 is a constant, and B_i , B_{ii} , B_{ij} are regression coefficients of the model, x_i and x_j are the
168 independent variables in coded values, and k is the number of factors.

169 Shapiro-Wilk test was used to evaluate normality of the data, while the possible presence of outliers
170 and the homogeneity of variance were evaluated by residual analysis. Goodness of fit was measured
171 with the adjusted determination coefficient (R^2_{adj}). p -Values for the coefficients of the response
172 surface were defined using standard t -test. Three-dimensional counter plots were drawn to illustrate
173 the effects of the considered factors on the responses. To this purpose, the values of the response
174 were plotted on the z -axis against the two most relevant factors, keeping the third one fixed to a
175 constant value (the central one).

176 Results relevant to preliminary trials are the average of at least three measurements carried out on
177 two replicated experiments. Data are reported as mean value \pm standard deviation. Statistical
178 analysis was performed by using R v. 2.15.0 (The R Foundation for Statistical Computing).
179 Bartlett's test was used to check the homogeneity of variance, one way ANOVA was carried out
180 and Tukey test was used to determine statistically significant differences among means ($p < 0.05$).

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182 **3. Results and discussion**

183 *3.1. Individual vs combined US-HPH nanoemulsification preliminary trials*

184 Preliminary trials were performed to assess the capability of US-HPH combined processes to
185 produce nanoemulsions containing 2% (w/w) Tween 80 or whey protein isolate, as emulsifiers, in
186 comparison to US and HPH individual treatments. In particular, the combined US-HPH processes
187 consisted of 20 s or 60 s US followed by HPH process at 20, 50, 80 and 100 MPa. The reverse
188 process (HPH-US) was not considered based on previous results highlighting that only US before
189 HPH allowed the efficacy of combined process to be improved (Calligaris et al., 2016). The
190 individual US treatments were conducted for 20 to 240 s, whereas HPH homogenization was
191 performed by increasing pressure from 20 to 150MPa for 1 pass, and at 120 MPa for 3 passes. The
192 energy densities provided by the combined treatments to the samples ranged from 20 to 360 MJ/m³
193 (Table 2). Figure 1 shows the particle size distributions of emulsions stabilized by Tween 80 or
194 whey protein isolate obtained by means of the combined US-HPH as well as single US and HPH
195 processes.

196 US-HPH processes allowed obtaining monomodal distributions using both emulsifiers at US times
197 and pressure levels as low as 20 s and 50 MPa, respectively (Figures 1a and 1b). It must be noted
198 that monomodal distributions were also obtained in both Tween 80 and whey protein isolate
199 stabilized emulsions by means of 240 s US (278 MJ/m³) and HPH at pressure higher than 80 MPa
200 (80 MJ/m³) (Figures 1c, 1d, 1e and 1f). The particle distribution amplitude and the mean particle
201 diameter decreased with the increase in the energy density provided to samples, as well evidenced
202 by the distribution width, the mean particle diameter value and the corresponding polydispersity
203 index (PDI) (Figure 1, Table 2). In the energy density range of 78-125 MJ/m³, particles with
204 diameter of about 220 nm and 300 nm were obtained using Tween 80 and whey protein isolate,
205 respectively (Table 2). Combined treatments at energies of 155-175 MJ/m³ further reduced the
206 distribution width and particle dimensions below 220 nm (Figure 1, Table 2). It is noteworthy that
207 diameters in the same order of magnitude were obtained only by applying 3 passes HPH at 120
208 MPa, corresponding 360 MJ/m³ of energy density (Table 2). Such high energy levels pose different
209 issues, including rapid wear and tear of plants and high energy consumption, which, in turn,
210 increase process costs and reduce process sustainability and industrial feasibility (Yang, Marshall-
211 Breton, Leser, Sher, & McClements, 2012). By contrast, results of the study showed that the
212 combination of US and HPH actually led to produce Tween 80 and whey protein isolate stabilized
213 nanoemulsions at energy densities lower than those required by the individual treatments.
214 Synergistic homogenization effects of US and HPH have been previously attributed to the effect of
215 the sequential application of different emulsification processes (Calligaris et al., 2016). In particular,

216 | the first homogenization by US would reduce particle dimension and distribution width_of the
217 | coarse emulsion favouring_the further droplet break-up in the second HPH step (Abbas et al., 2013;
218 | Calligaris et al., 2016; Pandolfe, 1995). Results of this study also shows that within each
219 | emulsifying process, the distribution width and the mean particle diameter of Tween 80 containing
220 | emulsions was lower than that of whey protein isolate containing ones (Figure 1, Table 2). This can
221 | be attributed to the chemical features of the considered emulsifiers and their ability to absorb on oil-
222 | water interfaces. Being Tween 80 a small non-ionic surfactant, it can rapidly adsorb to the oil-water
223 | interface during high-energy emulsification leading to the formation of small particles (Amani,
224 | York, Chrystyn, & Clark, 2009; Ghosh, Mukherjee, & Chandrasekaran, 2013). On the contrary, due
225 | to their high molecular weight, globular whey proteins are expected to slowly cover oil droplet
226 | surface generated during the high-energy emulsification process (Adjonu, Doran, Torley, &
227 | Agboola, 2014; Dissanayake & Vasiljevic, 2009; O'Regan & Mulvihill, 2010; Pearce & Kinsella,
228 | 1978).

230 3.2. Identification of the best US-HPH emulsifying conditions

231 To define the best performing process conditions to obtain nanoemulsions at the lowest energy
232 level, a three factors face centred central composite design (CCF) was used. To this aim, the oil
233 content, emulsifier concentration and emulsification energy density were considered as independent
234 variables and their effect on emulsion mean particle diameter was studied (Table 1). According to
235 the results of the preliminary trials, US-HPH treatments were applied to provide samples with low-
236 medium energy densities. Table 1 also shows the mean particle diameter of emulsions obtained
237 | under the different CCF conditions. The regression coefficients and the relative analysis of variance
238 | of the polynomial models for the dependent variables are presented in Table 3. R^2_{adj} values for the
239 responses were higher than 0.894.

240 The results showed that linear and quadratic terms of energy density (E_v and E_v^2 , respectively), and
241 linear terms of oil (*Oil*) and emulsifier (*Emuls*) contents had significant effects on mean particle
242 diameter of Tween 80 stabilized emulsions, showing *p*-values lower than 0.001. Similarly, energy
243 density (both linear and quadratic term) and oil content (linear term) significantly affected droplet
244 dimensions of whey protein stabilized emulsions ($p < 0.001$, 0.01 and 0.05, respectively).

245 To evaluate the effects of the independent variables on the dependent one and to predict the
246 optimum values of each variable for minimum mean droplet diameter to be achieved, contour-plots
247 were generated. Figure 2 shows the contour-plots relevant to the effect of energy density and oil
248 | content (Figure 2a) or surfactant content (Figure 2b) on particle dimensions of Tween 80 stabilized
249 | emulsions. Nanoemulsions with the lowest diameter were obtained at the highest energy -densities

250 and were associated to the lowest oil content (Figure 2a). In particular, the mean particle diameter
251 decreased from about 400 nm to less than 160 nm as the energy density of the treatment increased.
252 This indicated that the progressive enhancement of disruptive forces at the homogenization valve
253 led to the generation of particles getting smaller due to the rapid absorption of Tween 80 at the
254 oil/water interface. As the oil content increased at constant emulsifier level, the mean particle
255 diameter also increased. It is likely that the passage at the homogenization valve of a higher
256 quantity of oil reduced the efficacy of the treatment being the energy delivered to be shared between
257 an increased oil quantity at a constant emulsifier concentration. Moreover, the surfactant content (2
258 % w/w) could be not enough to surround all the newly formed oil droplets. This observation is
259 supported by results reported in Figure 2b, showing the mean particle diameter of Tween 80
260 stabilised emulsions as a function of energy density and emulsifier content, while maintaining oil
261 content constant at 15 % (w/w). In fact, increasing the Tween 80 level produced a significant
262 decrease in oil droplet dimensions.
263 Different behaviour was observed for whey protein stabilized emulsions (Figure 3). The minimum
264 oil droplet diameter was achieved by transferring to the 10% (w/w) oil emulsion intermediate
265 energies of about 110-140 MJ/m³ (Figure 3a). Beyond these energy values, a further decrease of
266 droplet size was not observed. Similar considerations can be also drawn by observing the plot of
267 mean droplet diameter as a function of whey protein content and energy density (Figure 3b), by
268 imposing 15% (w/w) value to the oil content variable. Also in this case, the best performing
269 conditions in terms of emulsion droplet size were achieved at intermediate energy densities. It is
270 possible that higher energy density values produced a progressive unfolding of whey proteins,
271 leading to a reduction of their emulsifying properties. -To this regard, different studies highlighted
272 the capability of HPH to modify the protein structure. In particular, Oboroceanu et al. (2011)
273 showed that high pressure microfluidization treatments (>50 MPa) of β -lactoglobulin induced 30%
274 protein denaturation, accompanied by changes in secondary structure. Similarly, Bouaouina,
275 Desrumaux, Loisel and Legrand (2006) reported that high pressure homogenization could modify
276 the structure of whey protein, exposing the buried hydrophobic residues. Moreover, a recent study
277 of Ali et al. (2018) reported HPH treatments to induced secondary structure transformation and
278 protein aggregation via intermolecular disulfide bridges. Additionally, observing Figure 3b, it can
279 be noted that whey protein isolate concentration did not to significantly affect the particle
280 dimensions. An amount of 1% (w/w) whey proteins resulted to be sufficient to stabilize oil-water
281 interface developed by the applied US-HPH combined treatments. Exceeding 1% (w/w) content,
282 proteins were likely to locate in the continuous aqueous phase rather than at the oil-water interface

283 (Yan, Park, & Balasubramaniam, 2017). Based on these considerations, whey protein content can
284 be minimized while maintaining good emulsification efficacy.

285 In the light of these results, the energy density developed by US-HPH process and the formulation
286 conditions allowing the minimum dimension of emulsion oil droplets to be obtained, were
287 estimated. For Tween 80 stabilized emulsions, 3% (w/w) emulsifier concentration, 10% (w/w) oil
288 content and at least 145 MJ/m³ energy density would guarantee emulsions with droplet diameter of
289 140-190 nm. In the case of whey protein stabilized emulsions, a minimum droplet size around 200-
290 250 nm can be achieved by supplying energy density values lower than 120 MJ/m³ to an emulsion
291 containing 10% (w/w) oil and 1% (w/w) emulsifier.

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293 3.3. *Effect of energy density share between US and HPH during combined emulsification* 294 *processes*

295 Different combinations of US time and HPH pressure can be employed to deliver the same energy
296 density during a US-HPH process. For instance, 120 MJ/m³ can be transferred to the system by
297 applying 22 s+90 MPa, 44 s+60 MPa or 75 s+30 MPa. Therefore, the last part of the research aimed
298 to study the effect of the ratio between US and HPH in delivering the energy density during US-
299 HPH nanoemulsification. The total energy densities, oil and emulsifier contents were selected based
300 on CCF results as those allowing the lowest nanoemulsion droplet diameter to be generated. Energy
301 density, oil content and emulsifier concentrations were 145 MJ/m³, 10% (w/w) and 3% (w/w) for
302 the Tween 80 containing system; 120 MJ/m³, 10% (w/w) and 1% (w/w) for whey protein isolate
303 containing one. The selected energy densities were, then, provided by using different combinations
304 of US time and HPH pressure, progressively increasing the energy share generated by US and
305 concomitantly reducing the one delivered by HPH, as shown in Table 4.

306 All combined processes resulted in lower particle dimensions than the corresponding individual
307 homogenization treatments delivering the same energy density, in agreement with the CCF data [and](#)
308 [previously reported results \(Calligaris et al., 2016\)](#). In particular, in the case of Tween 80 containing
309 emulsions, the combinations in which 50-75% of the total energy density was delivered by HPH
310 and the remaining energy by US, resulted in particle diameters in the range of 150-170 nm. It is
311 noteworthy that an increase in energy share delivered by US (75%), with a concomitant reduction of
312 HPH-delivered one (25%), produced larger diameters, confirming the higher emulsification efficacy
313 of HPH as compared to US. Similarly, in the case of whey protein isolate stabilized emulsions,
314 lower diameters were observed when at least 50% of total energy share was delivered by HPH.
315 These treatments, in fact, allowed particles with mean diameters of about 230 nm to be obtained,
316 again validating the CCF model. [It can be concluded that the high pressure homogenization step of](#)

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317 the combined process has to be considered the critical phase to obtain fine emulsions. The US
318 treatment before HPH would prevalently serve to reduce particle size and distribution width of the
319 coarse emulsion before entering in the homogenization valve. In other words, the US step would
320 improve the efficiency of the second HPH homogenization in obtaining particles even lower.

322 **Conclusions**

323 In this work, the efficacy of combined US-HPH emulsification processes at low energy density to
324 obtain nanoemulsions was demonstrated. Moreover, the proposed combined nanoemulsification
325 appears to be versatile, since it can be exploited by using different levels of both Tween 80 and
326 whey protein isolate as emulsifiers as well as oil at different contents. Depending on the emulsifier
327 used in the formulation, the best performing processing parameters (total energy density and energy
328 density share between US and HPH) and formulation conditions (oil and emulsifier contents) has to
329 be tested and defined. In fact, the emulsifier characteristics greatly affected -the performances of
330 combined US-HPH process. In all cases, the combined process led to nanoemulsions at energy
331 density levels which were approximately half of those required by single US or HPH to obtain the
332 same emulsification performances in terms of mean particle diameter.

333 From an industrial perspective, these results open interesting possible opportunities in the attempt to
334 design more sustainable emulsification processes and devices. It should be stressed that
335 homogenization pressure lower than 60 MPa and ultrasonication duration of a few seconds appear
336 compatible with the actual industrial needs, leading to a possible reduction of the total ownership
337 cost. Finally, the proposed approach could definitively contribute to increasing the exploitability of
338 nanoemulsions in food at large-scale production facilities.

340 **Acknowledgements**

341 Authors are grateful to Dr. Annalisa Malchiodi and Dr. Silvia Grasselli of Gea Mechanical
342 Equipment Italia for technical support in HPH processing and to Dr. Federica Sfiligoi for
343 contributing to analyses.

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434 **Caption of Figures**

435 Figure 1. Particle dimension distributions of emulsions containing 2% Tween 80 (a, c, e) or whey
436 proteins (b, d, f), produced by means of US-HPH (20 s + 20 MPa, 20 s + 50 MPa, 60 s + 50 MPa
437 and 60 s + 100 MPa), US (20, 60, 120 and 240 s) and HPH (1 pass at 20, 80, 150 MPa and 3 passes
438 at 120 MPa) treatments.

439 Figure 2. Fitted contour plots of mean particle diameter of Tween 80 ~~(a) and whey protein (b)~~
440 stabilized emulsions as a function of energy density (E_v) and oil content (Oil) (a) or emulsifier
441 concentration (*Emuls*) (b). The value of the emulsifier concentration was kept at the central point
442 (2% w/w).

443 Figure 3. Fitted contour plots of mean particle diameter of ~~Tween 80 (a)~~ and whey protein ~~(b)~~
444 stabilized emulsions as a function of energy density (E_v) and oil content (Oil) (a) or emulsifier
445 concentration (*Emuls*) (b). The value of the oil content was kept at the central point (15% w/w).

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448 Table 1. Combinations of oil content, emulsifier concentration and energy density of different
 449 runs and experimental results \pm standard deviation of a three factors face centred central composite
 450 design

Run	Oil (% w/w)	Emulsifier (% w/w)	Energy density (MJ/m ³)	Mean particle diameter (nm)	
				Tween 80	Whey protein isolate
1	10	1	47	420 \pm 43	344 \pm 12
2	10	3	47	340 \pm 34	353 \pm 22
3	20	3	47	389 \pm 6	411 \pm 15
4	20	1	47	488 \pm 59	427 \pm 23
5	10	1	175	212 \pm 11	257 \pm 29
6	10	3	175	128 \pm 13	239 \pm 2
7	20	1	175	323 \pm 18	285 \pm 14
8	20	3	175	194 \pm 8	241 \pm 15
9	10	2	111	220 \pm 10	233 \pm 7
10	20	2	111	277 \pm 9	279 \pm 11
11	15	1	111	257 \pm 21	285 \pm 7
12	15	3	111	210 \pm 11	228 \pm 4
13	15	2	47	397 \pm 46	463 \pm 31
14	15	2	175	215 \pm 7	240 \pm 8
15	15	2	111	239 \pm 13	287 \pm 13
16	15	2	111	240 \pm 11	279 \pm 10
17	15	2	111	249 \pm 21	296 \pm 3
18	15	2	111	248 \pm 9	279 \pm 21
19	15	2	111	249 \pm 12	293 \pm 24
20	15	2	111	247 \pm 12	215 \pm 16

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451 Table 2. Mean particle diameter and polydispersity index (PDI) (\pm standard deviation) of emulsions containing 2% (w/w) Tween 80 or whey
 452 protein isolate, subjected to HPH and US provided in combination or individually at increasing energy density.

Treatment	Pressure (MPa)	Passes	Time (s)	Energy density (MJ/m ³)	Tween 80		Whey proteins	
					Mean particle diameter (nm)	PDI	Mean particle diameter (nm)	PDI
US-HPH	20		20	41	296 \pm 12 ^c	0.35 \pm 0.07 ^{cde}	430 \pm 9 ^b	0.54 \pm 0.08 ^b
	50		20	78	221 \pm 9 ^{ef}	0.24 \pm 0.04 ^{de}	291 \pm 3 ^{cd}	0.37 \pm 0.01 ^{bcd}
	80		20	108	208 \pm 11 ^{fgh}	0.28 \pm 0.00 ^{de}	304 \pm 10 ^{bc}	0.33 \pm 0.01 ^{bcd}
	50		60	125	225 \pm 12 ^{ef}	0.25 \pm 0.01 ^{de}	280 \pm 8 ^{de}	0.35 \pm 0.09 ^{bcd}
	80		60	155	194 \pm 10 ^{hi}	0.22 \pm 0.03 ^{ef}	218 \pm 1 ^{fg}	0.21 \pm 0.05 ^{fg}
	100		60	175	190 \pm 1 ^{hi}	0.17 \pm 0.01 ^f	205 \pm 5 ^{fg}	0.17 \pm 0.01 ^g
US			20	21	475 \pm 21 ^a	0.69 \pm 0.04 ^a	Phase separation	
			60	75	361 \pm 22 ^b	0.49 \pm 0.02 ^b	498 \pm 4 ^a	0.75 \pm 0.01 ^a
			120	143	385 \pm 10 ^b	0.49 \pm 0.03 ^b	441 \pm 17 ^{ab}	0.47 \pm 0.01 ^{bc}
			240	278	258 \pm 2 ^{cd}	0.38 \pm 0.04 ^{bc}	299 \pm 13 ^{bc}	0.42 \pm 0.03 ^{bc}
HPH	20	1		20	363 \pm 8 ^b	0.41 \pm 0.02 ^{cd}	389 \pm 15 ^b	0.43 \pm 0.01 ^{bc}
	50	1		50	265 \pm 12 ^{cd}	0.34 \pm 0.08 ^{cde}	292 \pm 13 ^{cd}	0.30 \pm 0.03 ^{cd}
	80	1		80	228 \pm 6 ^{ef}	0.27 \pm 0.01 ^{de}	250 \pm 14 ^{ef}	0.27 \pm 0.03 ^{ef}
	120	1		120	229 \pm 16 ^{ef}	0.26 \pm 0.06 ^{de}	243 \pm 7 ^{ef}	0.27 \pm 0.04 ^{ef}
	150	1		150	208 \pm 6 ^{fgh}	0.23 \pm 0.02 ^{ef}	245 \pm 13 ^{ef}	0.27 \pm 0.03 ^{ef}
	120	3		360	168 \pm 2 ⁱ	0.15 \pm 0.01 ^f	182 \pm 4 ^g	0.16 \pm 0.03 ^g

453 ^{a-i}: within each column, means with different letters are statistically different (p<0.05)

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455 Table 3. Regression coefficients of the models for mean particle diameter of emulsions stabilized
 456 with Tween 80 and whey proteins

Variable	Tween 80	Whey proteins
Intercept	637.167	261.447
E_v	-5.697 ***	-4.881 ***
E_v^2	0.018 ***	0.021 **
Oil	-2.880 ***	32.172 *
Oil ²	0.348	-0.680
Emuls	15.212 ***	83.995
Emuls ²	-6.873	-16.408
E_v x Oil	0.024	-0.044
E_v x Emuls	-0.070	-0.104
Oil x Emuls	-1.594	-1.297
R ² adj	0.981	0.894

*: $p < 0.05$; **: $p < 0.01$; ***: $p < 0.001$

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459 Table 4. Mean particle diameter obtained by the application of different combined US-HPH
 460 processes delivering energy densities of 145 and 120 MJ/m³ to systems containing Tween 80 and
 461 whey protein isolate, respectively.

Emulsifier	US time (s)	HPH pressure (MPa)	Total energy density (MJ/m³)	Energy delivered by US (%)	Energy delivered by HPH (%)	Mean particle diameter (nm)
Tween 80	0	145	145	0	100	278 ± 7 ^b
	26	109		25	75	170 ± 9 ^{de}
	50	73		50	50	151 ± 8 ^c
	90	36		75	25	196 ± 3 ^c
	100	0		100	0	389 ± 7 ^a
Whey proteins	0	120	120	0	100	342 ± 10 ^b
	22	90		25	75	228 ± 6 ^d
	41	60		50	50	231 ± 5 ^d
	75	30		75	25	270 ± 4 ^c
	81	0		100	0	386 ± 4 ^a

462 ^{a-c}: in the same emulsifier group, means with different letters are statistically different (p<0.05)

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Figure

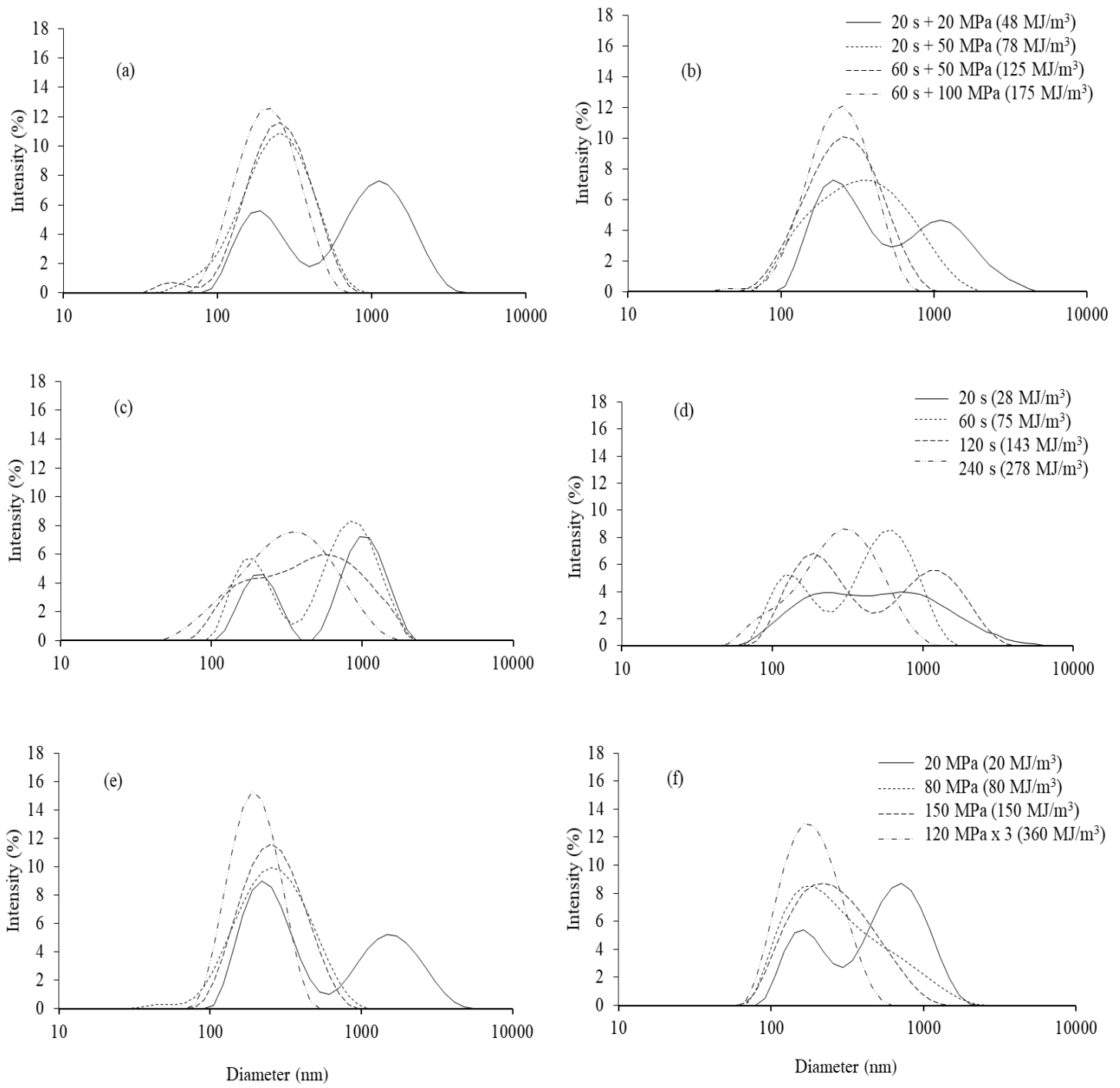


Figure 1.

Figure

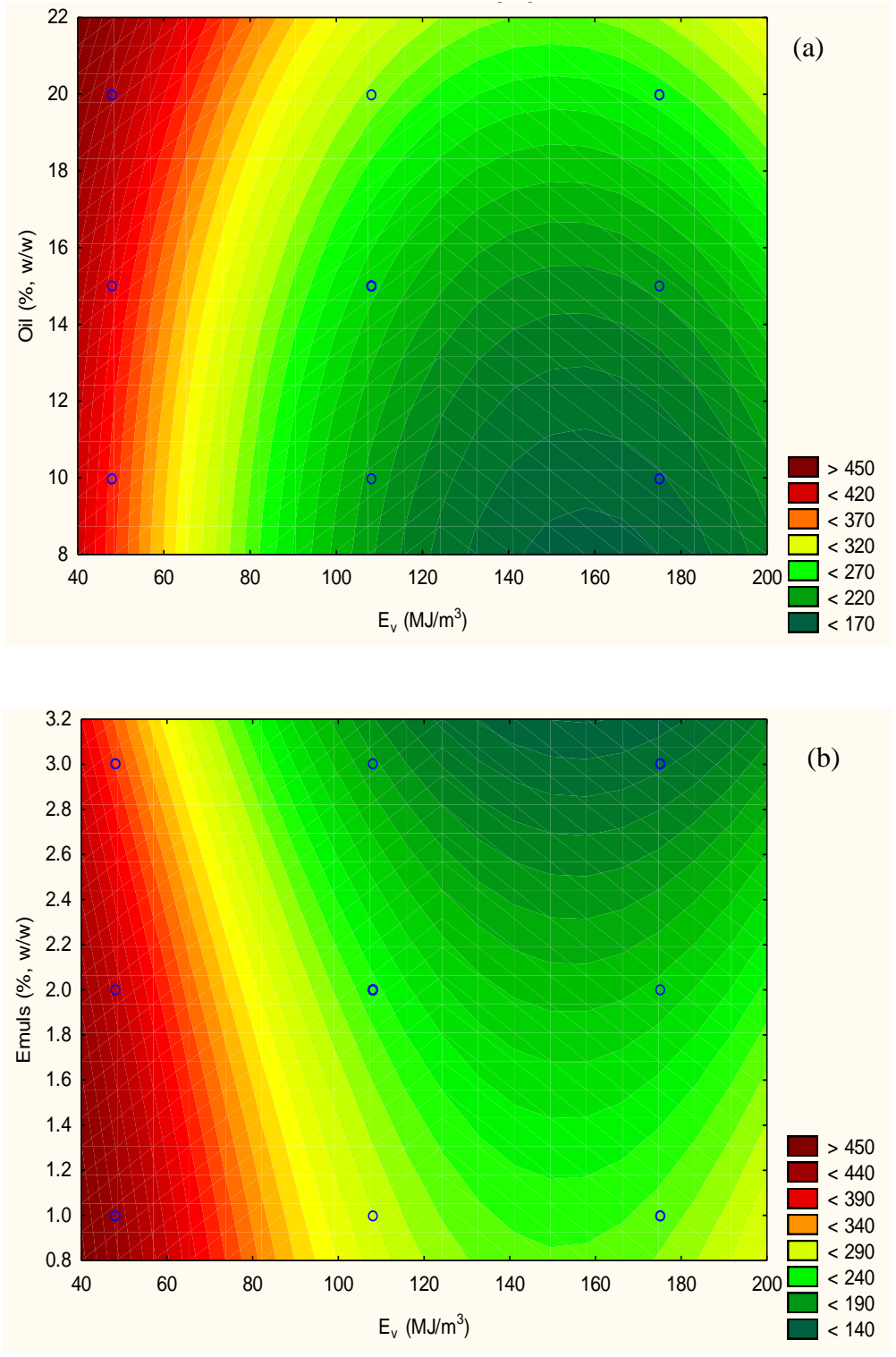


Figure 2.

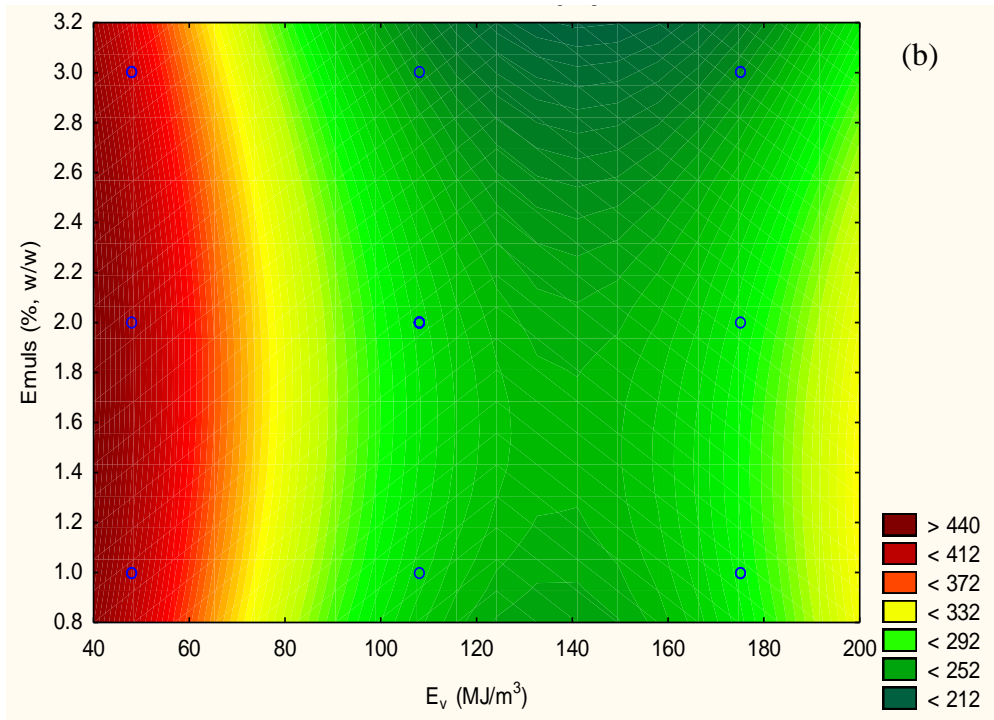
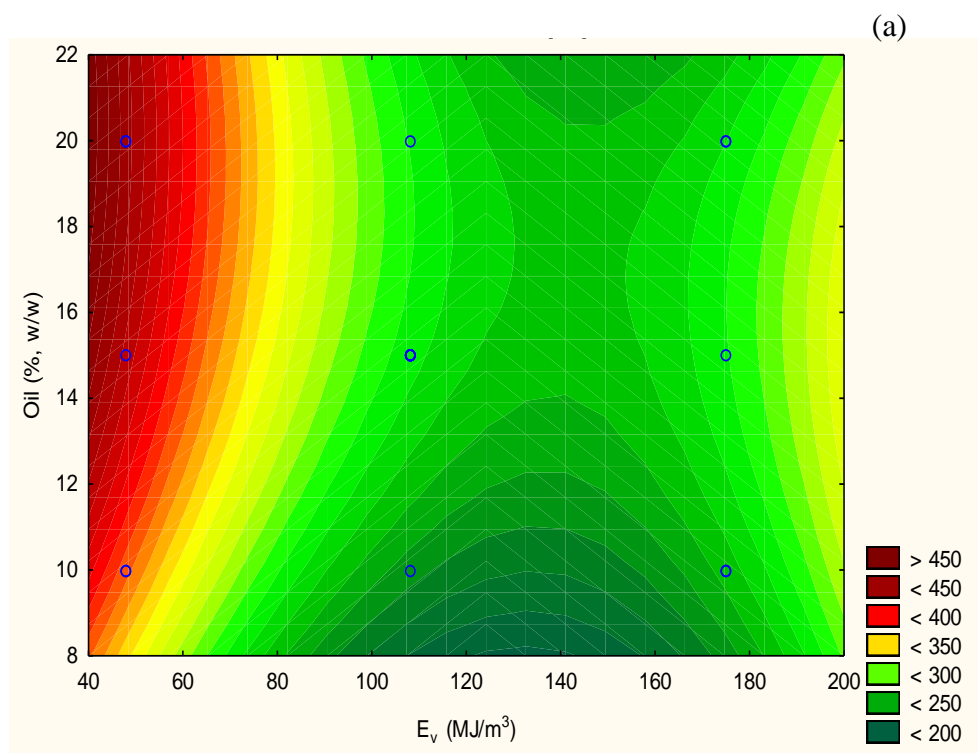


Figure 3.

